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  - Modeling of Water Networks
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  - Geomorphology



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# Bottom-Up Approach for Energy Balance of Water Distribution Pumping Station: Case Study from Bangkok, Thailand

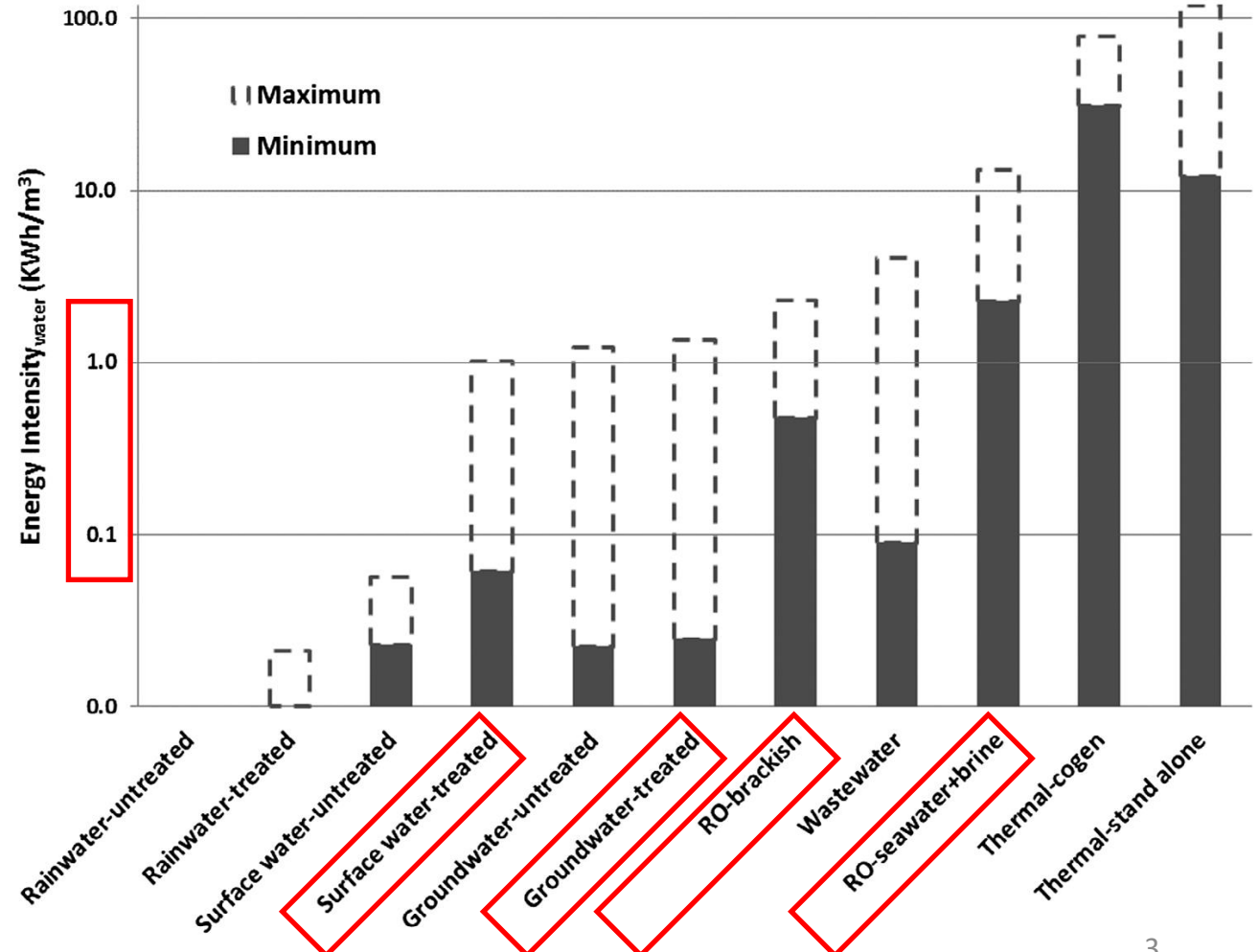
K. Wongpeerak, J. Changklom, S. Lipiwattanakarn and A. Pornprommin

in collaboration with Metropolitan Waterworks Authority (MWA),  
Thailand



# Energy used for water demand

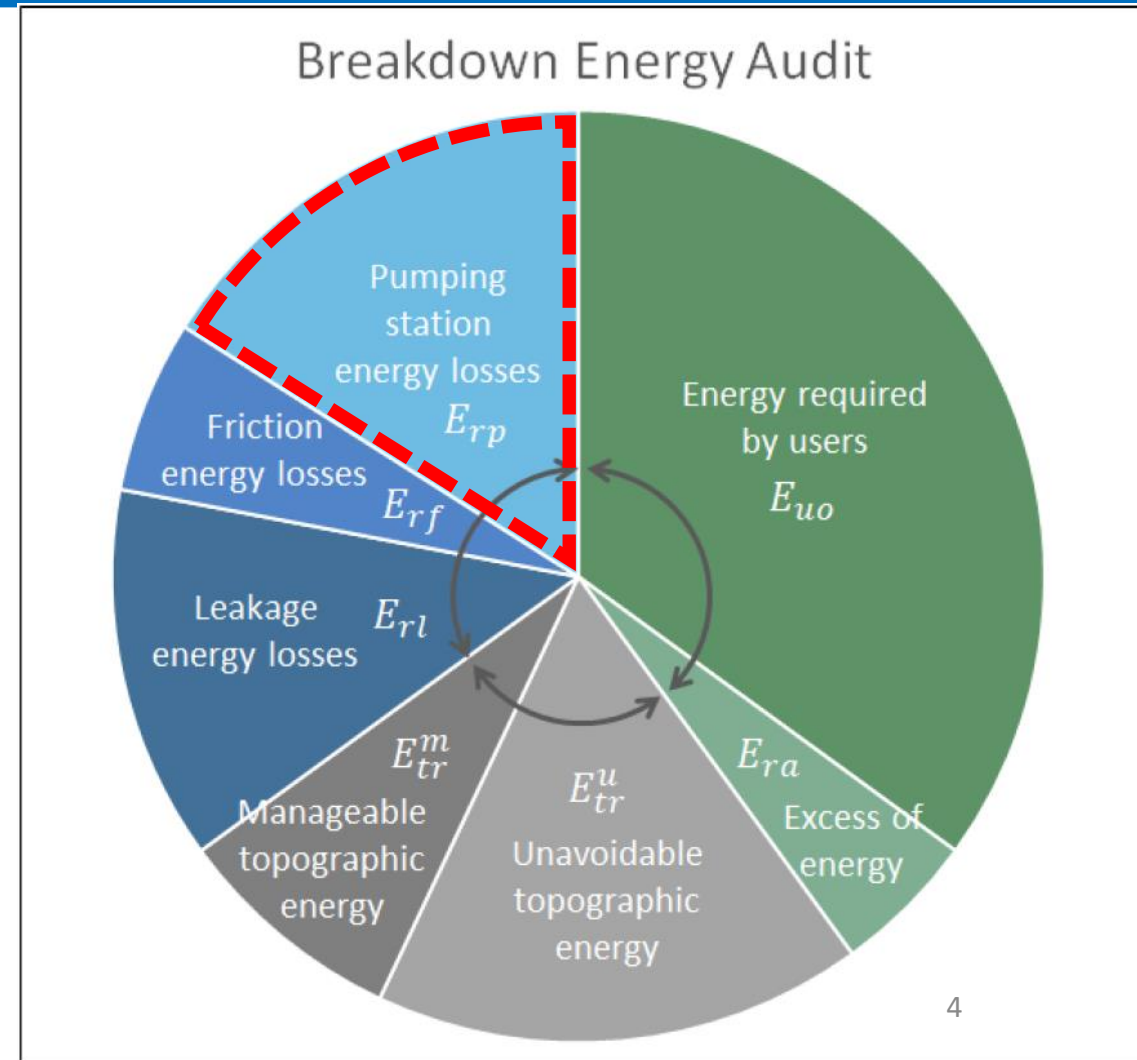
- Energy required for different water sources and extraction technologies.
- Treated surface water and groundwater consume less energy than RO.
- Magnitude of energy intensity is roughly in the order of 0.1 – 1 kWh/m<sup>3</sup>.
- Water transported over long distances is not considered due to difficulty!





# Energy audit for water transport

- According to waterworks processes, energy uses can be divided into
  - Raw water extraction
  - Water treatment
  - **Water distribution (or water transport)**
- This study focuses on the detailed pumping station energy loss ( $E_{rp}$ ) using EPANET model (Bottom-up Approach).





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# Metropolitan Waterworks Authority (MWA)

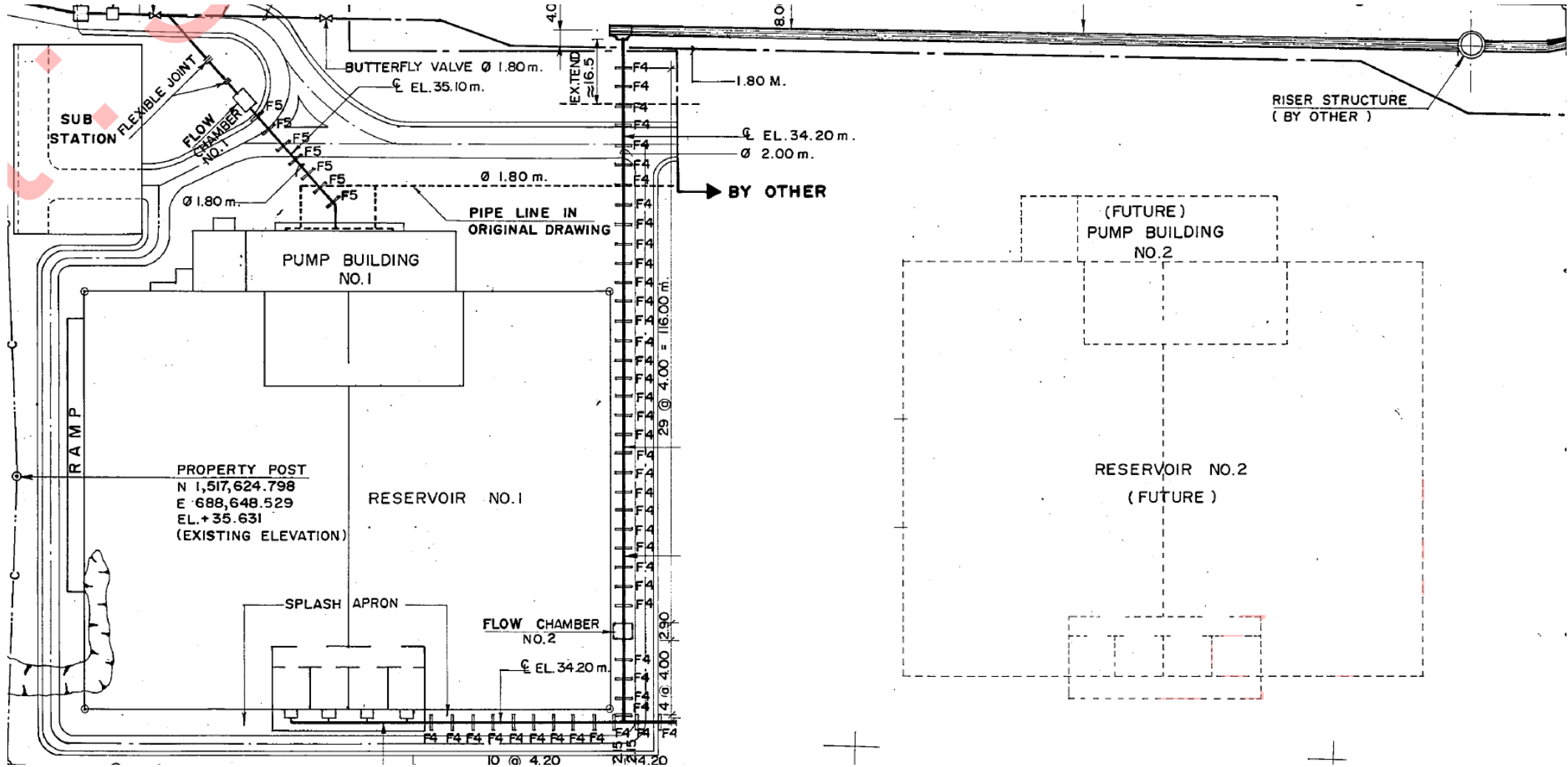


- A state enterprise under the Ministry of interior, Thailand
- Producing, distributing and selling treated water in 3 provinces:
  - Bangkok
  - Nonthaburi
  - Samutprakarn
- Service area of 2,500 km<sup>2</sup>
- Pipe length of 38,000 km
- 2.4 million customer connections
- Water production of 2 billion m<sup>3</sup>/ year
- Water consumption of 1.4 billion m<sup>3</sup>/ year



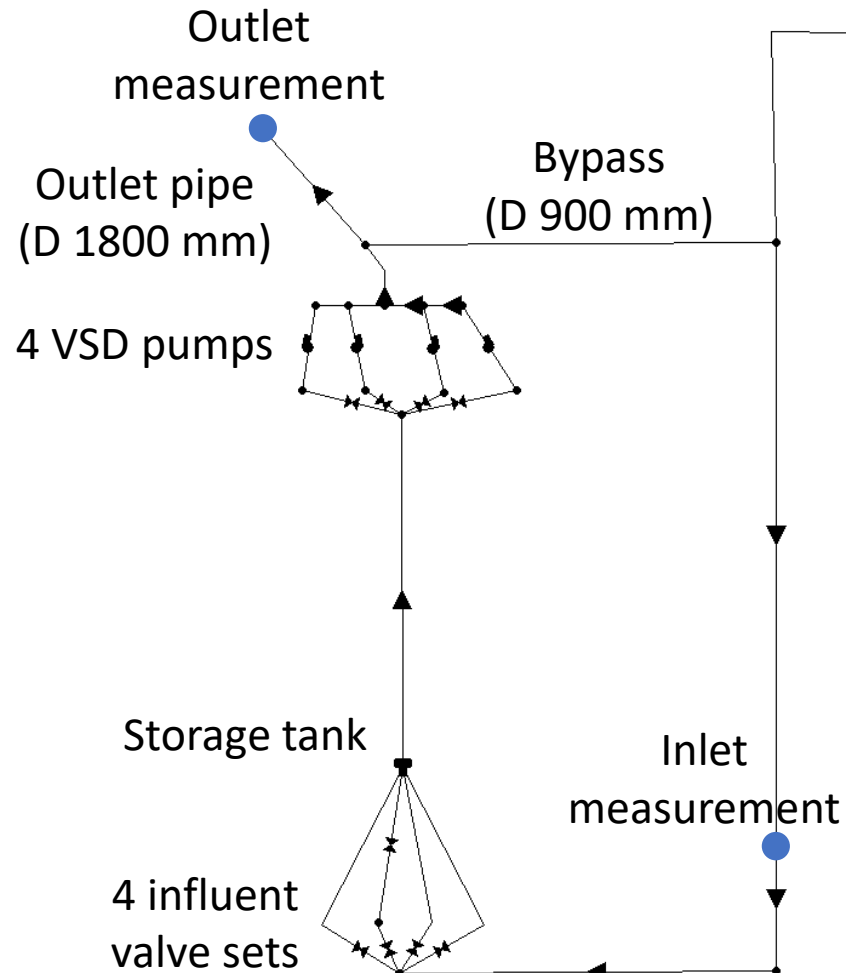


# Ladkrabang pumping station (LK PS) As-built drawing



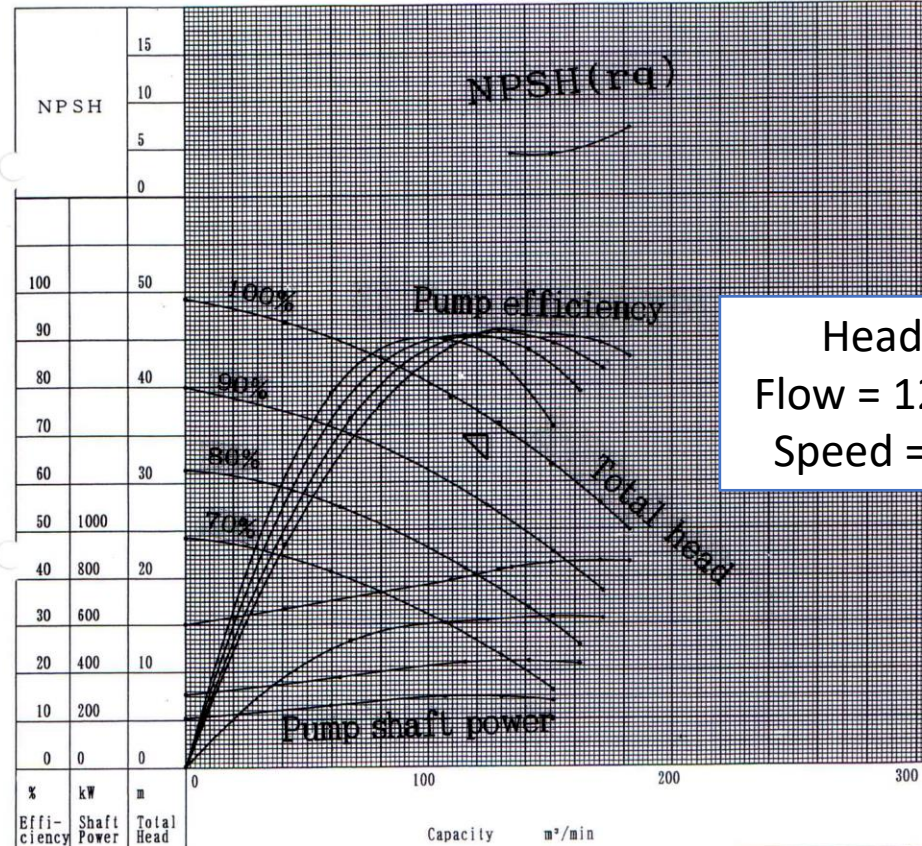


# EPANET model (extended period simulation)



Inlet pipe (D 2000 mm)

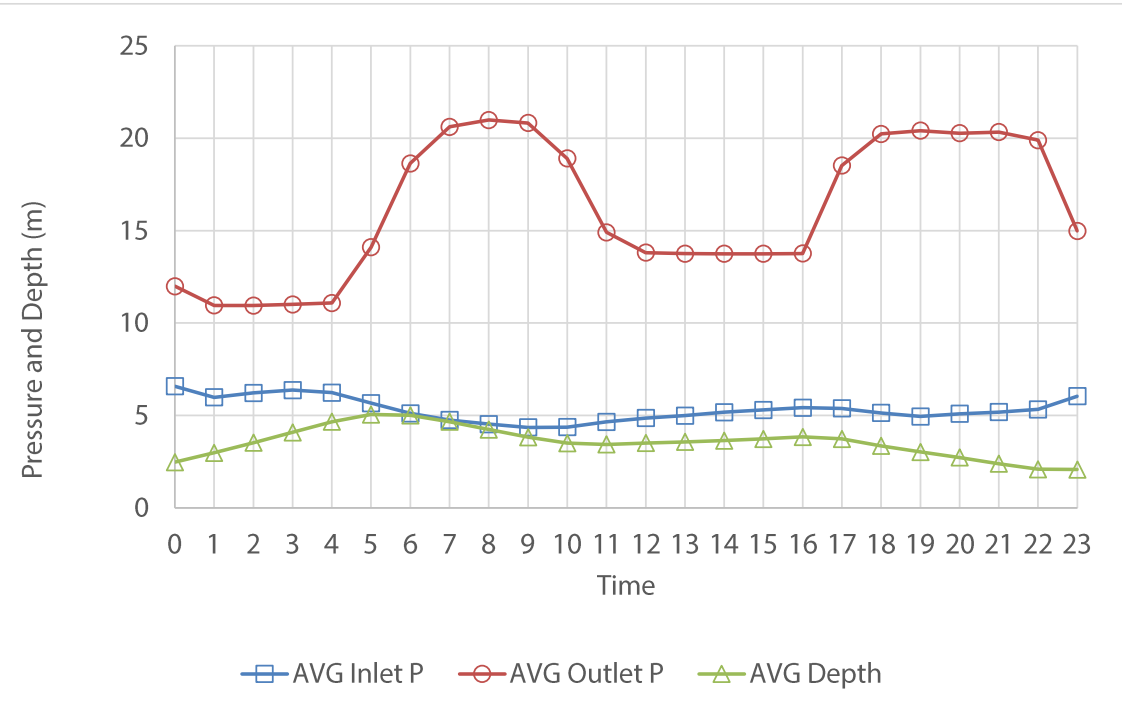
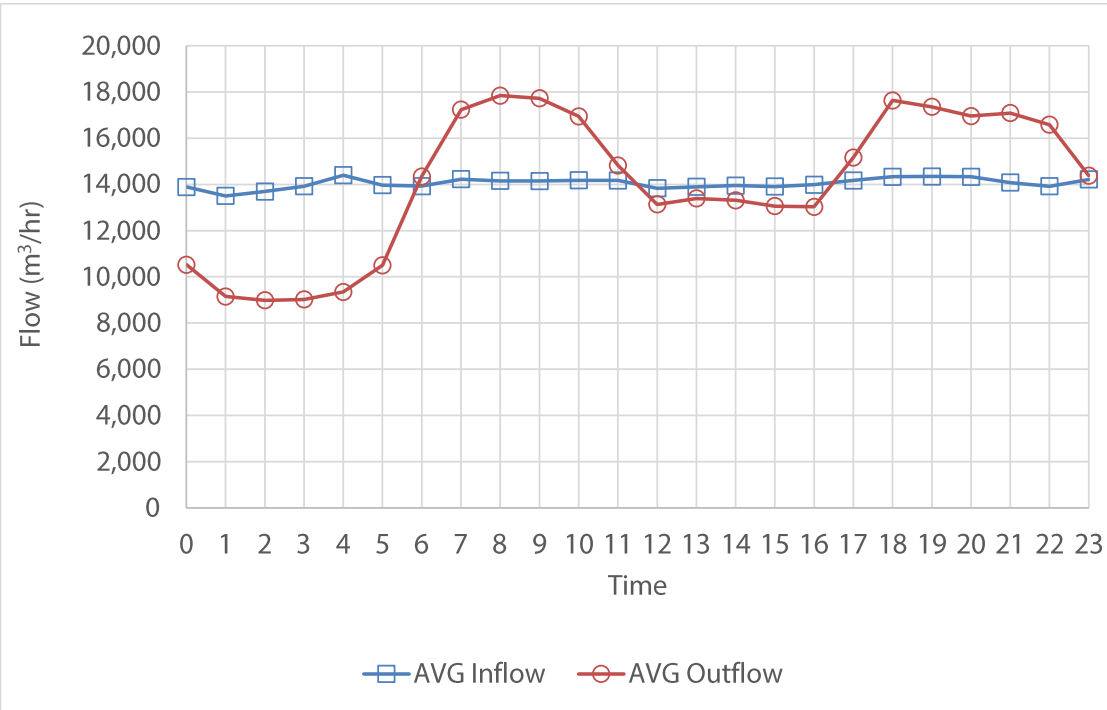
Riser from the tunnel



Head = 35m  
Flow = 125 m<sup>3</sup>/min  
Speed = 590 rpm



# Average hourly flow and pressure

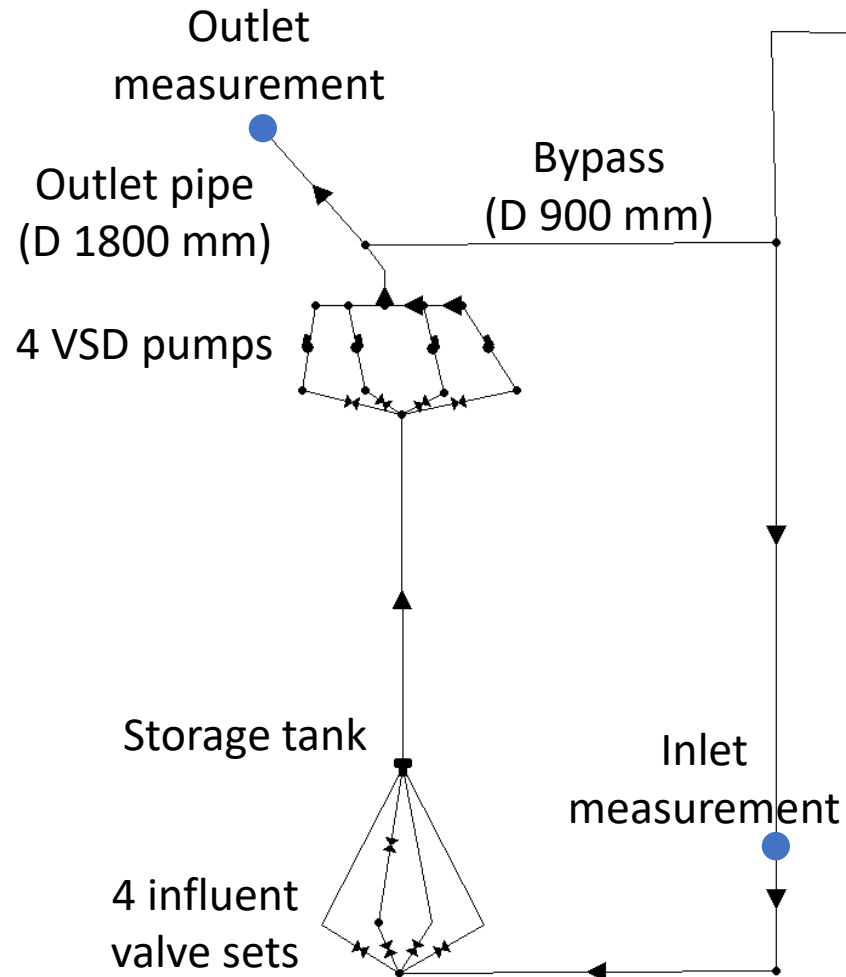


AVG Inflow = AVG Outflow = 14,000 m<sup>3</sup>/hr

AVG Inlet P = 5.3 m MSL  
AVG Outlet P = 16.2 m MSL  
AVG Water Depth in Tank = 3.5 m MSL  
Reference = Bottom of Tank = 0 m MSL



# Concept of Bottom-Up Approach for Energy Balance



		Riser from the tunnel	
	Inlet pipe (D 2000 mm)		
Input energy ( $E_{in}$ )	Natural input energy ( $E_{in,n}$ )	Energy delivered to outlet pipe ( $E_u$ )	
		Energy loss (EL)	Friction Energy of inlet pipe ( $EL_{f,in}$ )
	Energy loss by throttled influent valves ( $EL_{v,in}$ )		
	Energy loss by pump inefficiency ( $EL_p$ )		
Shaft input energy ( $E_{in,p}$ )	Friction Energy of outlet pipe ( $EL_{f,out}$ )		

# Energy balance calculation

- Natural input energy

$$E_{in,n}(t_p) = \gamma \cdot \sum_{i=1}^{n_N} \left[ \sum_{t_k=t_1}^{t_p} Q_{N_i}(t_k) \cdot H_{N_i}(t_k) \right] \cdot \Delta t$$

- Shaft input energy

$$E_P(t_p) = \gamma \cdot \sum_{i=1}^{n_P} \left[ \sum_{t_k=t_1}^{t_p} Q_{P_i}(t_k) \cdot H_{P_i}(t_k) / \eta_i(t_k) \right] \cdot \Delta t$$

- Energy delivered to outlet

$$E_U(t_p) = \gamma \cdot \sum_{i=1}^{n_{DM}} \left[ \sum_{t_k=t_1}^{t_p} q_{u_i}(t_k) \cdot H_{u_i}(t_k) \right] \cdot \Delta t$$

- Friction Energies of inlet and outlet pipes

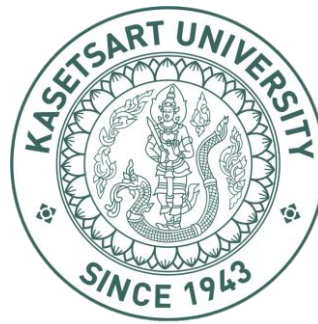
$$EL_F(t_p) = \gamma \cdot \sum_{i=1}^{n_p} \left[ \sum_{t_k=t_1}^{t_p} q_{p_i}(t_k) \cdot \Delta h_{p_i}(t_k) \right] \cdot \Delta t$$

- Energy loss by throttled influent valves

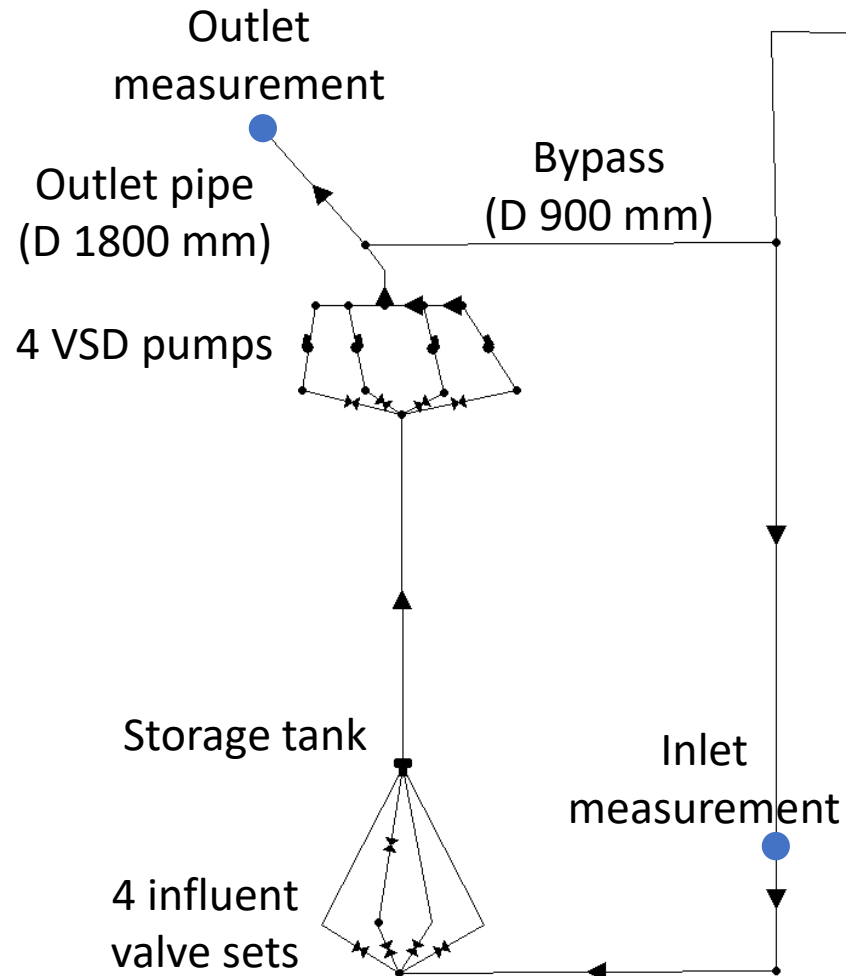
$$EL_V(t_p) = \gamma \cdot \sum_{i=1}^{n_V} \left[ \sum_{t_k=t_1}^{t_p} q_{V_i}(t_k) \cdot \Delta h_{V_i}(t_k) \right] \cdot \Delta t$$

- Energy loss by pump inefficiency

$$EL_P(t_p) = E_P(t_p) - \gamma \cdot \sum_{i=1}^{n_P} \left[ \sum_{t_k=t_1}^{t_p} Q_{P_i}(t_k) \cdot H_{P_i}(t_k) \right] \cdot \Delta t$$



# Energy Balance for April 2018



$E_{in}$ 24,400 (100)	$E_{in,n}$ 5,000 (20.5)	$E_u$ 17,200 (70.4%)	
	$E_{in,p}$ 19,400 (79.5)	$EL$ 7,200 (29.6)	$EL_{f,in}$ 1,400 (5.8)
			$EL_{v,in}$ 300 (1.2)
			$EL_p$ 3,900 (15.9)
$EL_{f,out}$ 1,600 (6.7)			

Units: kW.hr/day & (%)



# Discussion



Compute performance indices:

- Percentage of energy loss is  $EL/E_{in}$ 
  - $7,200/24,400 \times 100\% = 29.6\%$
- Energy intensity for water distribution is  $E_{in}/Q$ 
  - $24,400 \text{ kW.hr/day} \div 344,00 \text{ m}^3/\text{day} = 0.071 \text{ kW.hr/m}^3$
- Normalized energy intensity by pressure head is  $E_{in}/Q/P$ 
  - $0.071 \text{ kW.hr/m}^3 \div 16.2 \text{ m} = 0.0044 \text{ kW.hr/m}^3/\text{m}$
- Pump efficiency is  $1 - EL_p/E_{in,p}$ 
  - $(1 - 15.9/79.5) \times 100\% = 80\%$
- If LK PS is changed into a booster PS without a storage tank, it may save the energy roughly 1,700 kW.hr/day (7.0%) from a shorter inlet pipe, no throttled valves and tank, but the change will sacrifice water supply reliability.



# Conclusion



- The bottom-up approach for energy balance by EPANET model can support water companies to evaluate energy loss of each physical process.
- Performance indices can be used to improve the energy use and to compare with other waterworks utilities.



Thank you

